



# Mass transfer characteristics of a flow-by fixed bed electrochemical reactor composed of vertical stack stainless steel screens cathode

Ali H. Abbar<sup>1</sup> · Abbas H. Sulaymon<sup>2</sup> · Sawsan A. M. Mohammed<sup>3</sup>

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## Abstract

Mass transport properties of a flow-by fixed bed electrochemical reactor composed of a vertical stack of stainless steel nets operated at a batch-recycle mode were characterized using cathodic deposition of copper as a test reaction. The electrochemical reactor was operated at constant potential in which reduction of copper happened under mass transport control. This potential was selected from the application of hydrodynamic voltammetry using a borate/chloride solution as supporting electrolyte on stainless steel rotating disc electrode. A linear relationship was observed between the flow rate and the mass transfer coefficient. The electrochemical reactor was efficient in removing copper and able to reduce the levels of this metal to lower than 0.4 ppm starting from an initial concentration of 49.7 ppm at 80 min using a ratio of cathode volume/catholyte volume equal to 0.0075. A mathematical correlation between the Sherwood number and Reynolds number were obtained which characterized the mass transport properties of the reactor as follows:  $Sh = 0.2254Re^{0.4228}Sc^{1/3}$ .

## Nomenclature

a	Specific surface area $\text{cm}^2 \text{cm}^{-3}$	$I_L$	Limiting current mA
A	Cross sectional area of electrode $\text{cm}^2$	$j_D$	Chilton-Colburn j-factor –
b	Power of Reynolds Number in Eq. 10 –	$k_m$	Mass transfer coefficient $\text{cm s}^{-1}$
B	Opening size of screen cm	L	Length of electrode cm
C(0)	Initial Concentration at time = 0 $\text{mol.cm}^{-3}$ or ppm	$L_i$	Length of wire segment in Eq. (3-c) cm
C(t)	Concentration at time = t $\text{mol.cm}^{-3}$ or ppm	m	Constant in Eqs. 10 and 11 –
$C_b$	Bulk concentration $\text{mol.cm}^{-3}$ or ppm	N	Mesh size number Wire/in.
d	Diameter of wire screen cm	n	Power of Reynolds Number in Eq. 11 –
D	Diffusivity $\text{cm}^2 \text{s}^{-1}$	Q	Volumetric Flow rate $\text{cm}^3 \text{s}^{-1}$ or $\text{dm}^3 \text{h}^{-1}$
E	Cell potential mV	t	Time s
$E_{\max}$	Maximum electrode potential mV	u	Flow velocity of solution $\text{m s}^{-1}$
$E_{\min}$	Minimum electrode potential mV	$V_r$	Volume of reservoir $\text{cm}^3$
F	Faraday number(96500) $\text{C mol}^{-1}$	w	Thickness of electrode cm
i	Current density $\text{mA cm}^{-2}$	z	Number of electrons –
$i_{\text{lm}}$	Limiting current density $\text{mA cm}^{-2}$		

## Dimensionless numbers

Re	Reynolds number ( $Re = ud / \epsilon \nu$ ) –
Sh	Sherwood number dimensionless( $Sh = k_m d/D$ ) –
Sc	Schmidt number dimensionless( $Sc = \mu/\rho D$ ) –
X	Geometric dimensionless parameter –

## Greek symbols

$\rho$	Fluid density $\text{g cm}^{-3}$
$\mu$	Viscosity of fluid $\text{g m}^{-1} \text{s}^{-1}$
$\nu$	Kinematic viscosity of fluid $\text{cm}^2 \text{s}^{-1}$
$\epsilon$	Void fraction or porosity –
$\omega$	Rotation velocity $\text{rad s}^{-1}$

✉ Ali H. Abbar  
ali.abbar@qu.edu.iq; aliabbar68@yahoo.com

<sup>1</sup> Chemical Engineering Department, University of Al-Qadisiyah, Diwaniya, Iraq

<sup>2</sup> Refrigeration and Air –Conditioning Technical Engineering Department, College of Technical Engineering, The Islamic University, Najaf, Iraq

<sup>3</sup> Chemical Engineering Department, University of Baghdad, Baghdad, Iraq